

Thermal Conductivity of Methane

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This paper reports thermal conductivity data for methane measured in the temperature range 120–400 K and pressure range 25–700 bar with a maximum uncertainty of $\pm 1\%$. A simple correlation of these data accurate to within about 3% is obtained and used to prepare a table of recommended values.

KEY WORDS: methane; thermal conductivity; transport properties.

1. INTRODUCTION

Many measurements of the thermal conductivity of methane have been reported (Table I) [1–12]. A survey of the literature shows that few experiments have covered wide ranges of temperature and pressure. In this paper, measurements are reported in the range 120–400 K and 25–700 bar with a maximum uncertainty of 1%. It provides new measurements at low temperatures ($T < 300$ K) and high pressures ($P > 500$ bar) in addition to accurate second measurements in other regions.

A simple equation for the thermal conductivity of methane is proposed. The new correlation is used to prepare a table of recommended value that are accurate to within $\pm 3\%$.

2. EXPERIMENTAL

The measurements reported here are obtained with a transient hot-wire instrument described elsewhere [13]. The thermal conductivity cell con-

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Table I. Survey of Experimental Work on the Thermal Conductivity of Methane

| Ref. | Author(s) | Year | T (K) | P (bar) | Method |
|------|--------------------------|------|---------|-----------------------|----------------------|
| 1 | Borovik <i>et al.</i> | 1940 | 103–173 | Near saturated liquid | Concentric cylinders |
| 2 | Johnston and Grilly | 1946 | 96–385 | Atmospheric | Concentric cylinders |
| 3 | Keyes | 1954 | 120–273 | 1.1–9.0 | Concentric cylinders |
| 4 | Geier and Schafer | 1961 | 273–973 | Atmospheric | Concentric cylinders |
| 5 | Ikenberry and Rice | 1963 | 99–235 | 1.6–500 | Concentric cylinders |
| 6 | Golubev | 1963 | 196–508 | 1.0–608 | Concentric cylinders |
| 7 | Carmichael <i>et al.</i> | 1966 | 278–411 | 1.0–345 | Concentric spheres |
| 8 | Misic and Thodos | 1966 | 275–348 | 1.0–585 | Concentric cylinders |
| 9 | Rosenbaum and Thodos | 1967 | 336–435 | 3.8–697 | Concentric cylinders |
| 10 | Le Neindre <i>et al.</i> | 1969 | 298–725 | 1.0–1247 | Concentric cylinders |
| 11 | Sokolova and Golubev | 1967 | 109–239 | 1.0–500 | Regular regime |
| 12 | Gonzales <i>et al.</i> | 1968 | 122–173 | 5.0–100 | Axial flow cylinder |

sisted of a platinum wire 25 μm in diameter. Potential leads were welded onto the main wire to provide a test section of about 8.7 cm.

The platinum wire was stretched vertically in the test fluid and electrically heated with a step current from zero time. To a first approximation, the wire simulated an infinite line source with constant heat dissipation and the conductivity was calculated [14] from the temperature rise ΔT_w of the wire between times t_1 and t_2 according to the following equation⁴:

$$\Delta T_w(t_1, t_2) = (Q_l/4\pi\lambda)\ln(t_2/t_1) \quad (1)$$

The transient response of the wire was recorded by a computerized data acquisition system. Apparent thermal conductivities at increasing times were computed and a true conductivity estimated by extrapolation to zero time with the condition [15]

$$\left. \frac{d\lambda}{dt} \right|_{t=0} = 0 \quad (2)$$

Corrections for the finite heat capacity of the wire and nonconstant heat dissipation were applied during data processing.

3. RESULTS

The thermal conductivity of methane was measured along 15 nominal isotherms from 120 to 400 K at 20 K intervals. In all, 180 measurements are reported (Appendix, Table IV). Density ρ ($\text{g} \cdot \text{cm}^{-3}$) at the stated tempera-

⁴For an explanation of symbols, see nomenclature at the end of the paper.

ture T (K) and pressure P (bar) are obtained [16] and tabulated in addition to the thermal conductivity values λ ($\text{mW} \cdot \text{m}^{-1} \cdot \text{K}^{-1}$).

The accuracy and reproducibility of the apparatus were estimated to be within 1 and 0.5%, respectively.

The methane sample used in the experiment was supplied by Air Products and Chemicals Inc., Pennsylvania, and was of CP grade with a certified purity of better than 99%. The purity of this sample was tested in a mass spectrometer.

4. CORRELATION AND DISCUSSION

4.1. General Correlation

The thermal conductivity model (Fig. 1) suggested by Sengers *et al.* [17] and employed by us in a previous correlation of the data for ethane [18] was used with

$$\lambda(\rho, T) = \lambda_{\text{bg}}(\rho, T) + \Delta\lambda_{\text{cr}}(\rho, T) \quad (3)$$

$$\lambda_{\text{bg}}(\rho, T) = \lambda_1(T) + \Delta\lambda_e(\rho, T) \quad (4)$$

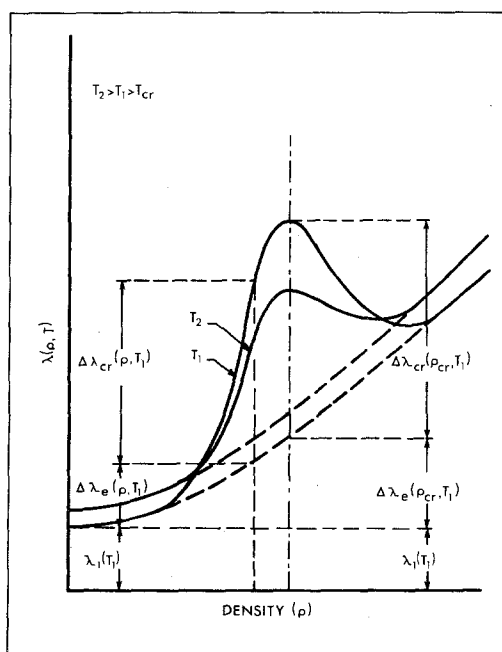


Fig. 1. The thermal conductivity model.

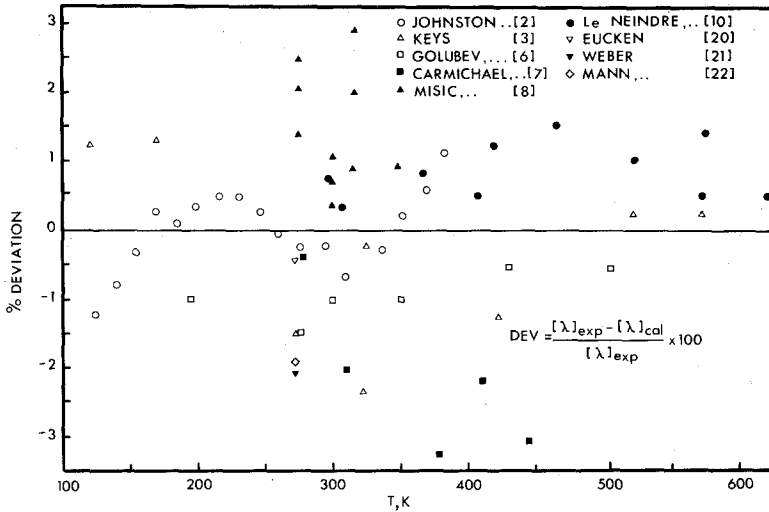


Fig. 2. Deviation plot: correlation of the thermal conductivity of methane at 1 bar.

4.2. Thermal Conductivity at 1 Bar

The hot wire utilized in this experiment closely approximated an ideal line source in the dense region. In the low-density region, however, the minimum-length criterion [19] was not satisfied and resulted in a high slope of the apparent thermal conductivity as a function of time. Extrapolation to zero time was not utilized in these cases due to high uncertainty in the extrapolated values. Consequently, measurements in the low-density region were not obtained with this cell.

Data in the low-density region ($P < 1.5$ bar, $120 < T < 622$ K) re-

Table II. Parameters of the Equations for the Thermal Conductivity of Methane

(A) Correlation for $\lambda_1(T)$ in the range of 120–622 K with Eq. (5):

$$n = 3 \quad a_0 = -0.47313668 \times 10^{-2}$$

$$a_1 = 9.35882659 \times 10^{-2}$$

$$a_2 = -5.37104001 \times 10^{-2}$$

$$a_3 = 1.32157337 \times 10^{-2}$$

(B) Correlation for $\Delta\lambda_e$ as a function of density with Eq. (6):

$$k = 1, 2, 5 \quad b_1 = 15.94004983$$

$$b_2 = 10.20614596$$

$$b_3 = 0.47065428$$

ported by other investigators [2, 3, 6–8, 10, 20–22] were correlated with [17]

$$\lambda_1(T) = \sqrt{T_r} / \sum_{k=0}^n (a_k / T_r^k) \quad (5)$$

This model is consistent with the theory [23] as well as with experimental evidence [17, 24] that the thermal conductivity of fluids in the low-density region depends only on temperature and not on density.

A correlation within 3% (Fig. 2) was obtained with Eq. (5) with $n = 3$ using the critical parameters from Ref. 16. Least square estimates of the parameters a_k are listed in part A of Table II.

4.3. The Excess Thermal Conductivity $\Delta\lambda_e$

The measurements in the high-density region indicated an increase in excess thermal conductivity $\Delta\lambda_e$ with increase in density along any isotherm. A thermal conductivity anomaly was observed in the critical region in a few measurements along the 200–300 K isotherms. These measurements were obtained in regions far from the critical point ($T_{cr} = 190.55$ K, $P_{cr} = 48.988$ bar, $\rho_{cr} = 0.16043$ g · cm⁻³) [16] and consequently only a weak anomalous effect is noticed.

On the basis of a preliminary analysis, eight measurements showing critical region enhancement and some in the low-density region were excluded from the data set for general correlation. In addition, it was necessary to include other available experimental data [3, 5–10] at low and moderate pressures in the region $\rho < 0.66$ g · cm⁻³.

The excess thermal conductivity $\Delta\lambda_e$ was first correlated with density alone with

$$\Delta\lambda_e(\rho) = \sum_k b_k \rho_r^k, \quad b_0 = 0 \quad (6)$$

A stepwise regression analysis of the data was performed. The best three-parameter model with $k = 1, 2, 5$ was selected and least square estimates of b_k were obtained (part B of Table II). A correlation of the present data to within 2–3% and a correlation of the other data within 4% was obtained with Eqs. (5) and (6). Figure 3 shows the deviation plot. This figure shows a dependence of $\Delta\lambda_e$ on temperature. Therefore, a correlation in terms of density and temperature was attempted with

$$\Delta\lambda_e(\rho, T) = \sum_{i=0}^m \sum_{j=0}^n b_{ij} T_r^i \rho_r^j, \quad b_{00} = 0 \quad (7)$$

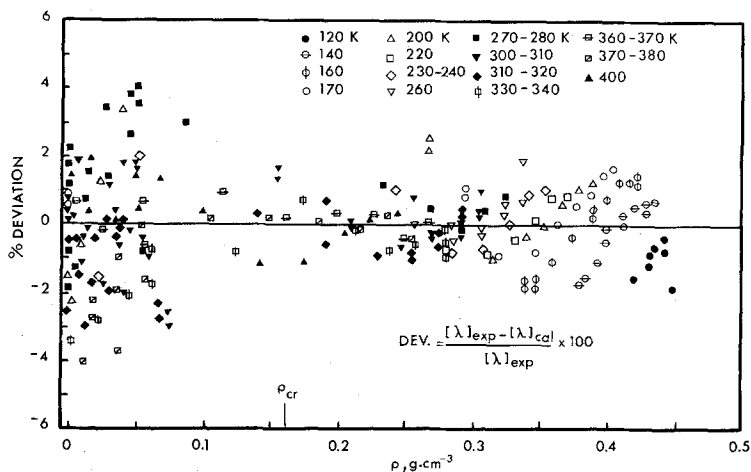


Fig. 3. Deviation plot: correlation of the thermal conductivity of methane.

Although this model matched the experimental data accurately, it did not properly estimate the background thermal conductivity values along various isotherms. Equation (6) was thus preferred over Eq. (7) for the general correlation of $\Delta\lambda_e$.

4.4. The Anomalous Thermal Conductivity $\Delta\lambda_{cr}$

A weak critical anomaly was observed in eight measurements. Table III shows these data and the magnitude of the critical region enhancement. A survey of the available experimental data indicated only a few data in the anomalous region. It was therefore not possible to establish an equation for $\Delta\lambda_{cr}$ in terms of density and temperature similar to that in Ref. 18.

5. DISCUSSION AND COMPARISON

The thermal conductivity calculated from the present correlation [Eqs. (5) and (6)] was compared with other experimental data [3, 4-10]. The data of Le Neindre *et al.* [10] show agreement within $\pm 2\%$ along all the isotherms in the range 300-650 K up to 700 bar (Fig. 4). Deviations of 4% are observed only along the 300 K isotherm in the near-critical density region. Along the 725 K isotherm and at pressures above 700 bar, the deviations are about 5%. The measurements of Keyes [3] agree to within 2% (Fig. 5). Deviations of other experimental data are also shown in Fig. 5. The deviations are generally within $\pm 2-3\%$ in the low-density region but increase somewhat in the dense-fluid region. Large systematic deviations of

Table III. Anomalous Thermal Conductivity of Methane

| ID# | T (K) | P (bar) | ρ (g · cm ⁻³) | λ_{exp} (mW · m ⁻¹ · K ⁻¹) | λ_{bg} (mW · m ⁻¹ · K ⁻¹) | $\Delta\lambda_{\text{cr}}$ (mW · m ⁻¹ · K ⁻¹) | $100\Delta\lambda_{\text{cr}}/\lambda_{\text{bg}}$ (%) |
|---------|----------|------------|-----------------------------------|---|--|--|---|
| CH4-069 | 199.99 | 50.86 | 0.0925 | 40.15 | 34.36 | 5.79 | 14.42 |
| CH4-077 | 220.03 | 100.84 | 0.1890 | 66.15 | 58.09 | 8.06 | 12.19 |
| CH4-164 | 260.71 | 200.96 | 0.2062 | 71.73 | 68.13 | 3.60 | 5.02 |
| CH4-165 | 260.90 | 150.90 | 0.1618 | 60.45 | 56.10 | 4.35 | 7.19 |
| CH4-166 | 261.15 | 200.96 | 0.2055 | 70.62 | 67.97 | 2.65 | 3.75 |
| CH4-167 | 261.17 | 100.84 | 0.1011 | 46.18 | 43.35 | 2.83 | 6.13 |
| CH4-175 | 278.28 | 200.89 | 0.1804 | 65.16 | 63.13 | 2.03 | 3.12 |
| CH4-176 | 278.52 | 150.90 | 0.1382 | 55.87 | 53.01 | 2.86 | 5.11 |

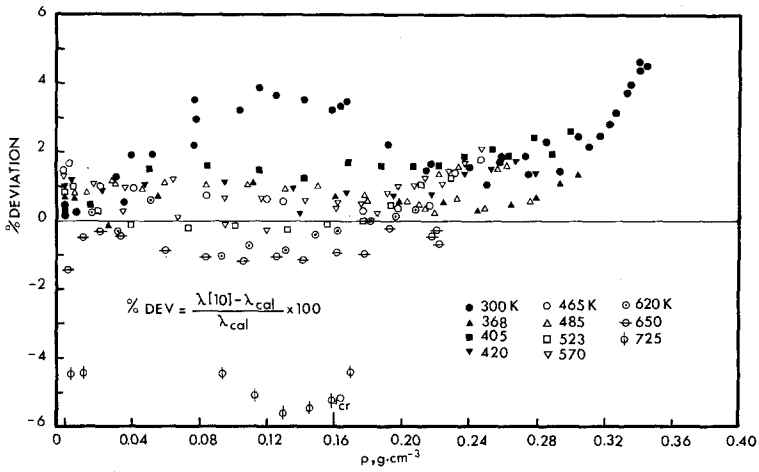


Fig. 4. Deviation plot of the thermal conductivity of methane: experimental data of LeNeindre *et al.* [10] and present correlation.

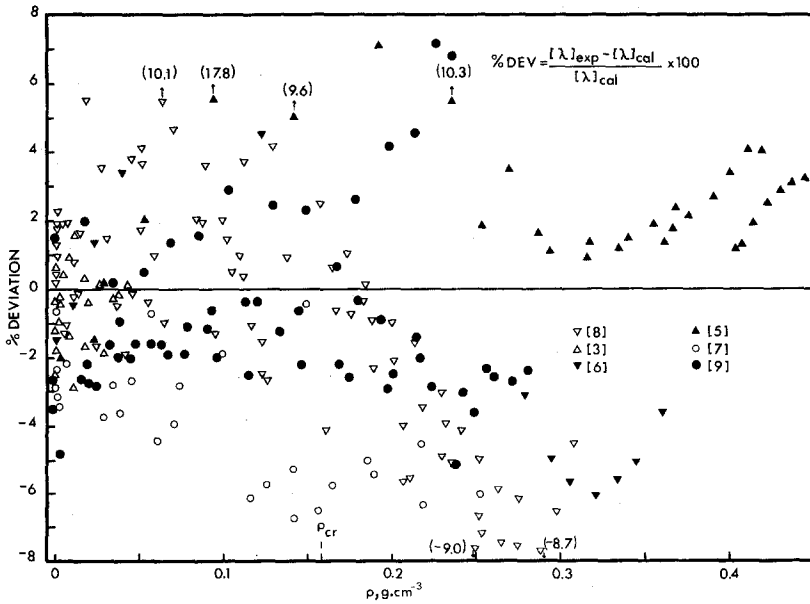


Fig. 5. Deviation plot of the thermal conductivity of methane: experimental data of Keyes [3]; Ikenberry and Rice [5]; Golubev [6]; Carmichael *et al.* [7]; Mistic and Thodos [8]; Rosenbaum and Thodos [9]; and the present correlation.

6–8% are observed for the data of Rosenbaum and Thodos [9] and of Misić and Thodos [8]. Some measurements of Ikenberry and Rice [5] indicate the anomalous effect of 7–18%, but in general these data agree within 3–4%. The measurements reported by Carmichael *et al.* [7] are consistently lower than the present correlation.

It is seen that the available thermal conductivity data in the low-density region are accurate. In the dense region, however, systematic errors are observed in some data. The present correlation has been developed on the basis of experimental data obtained in the dense region with a transient hot-wire apparatus. The accuracy of these measurements has been established by an error analysis [15].

In the absence of any equation for $\Delta\lambda_{cr}$, this correlation determines only the background thermal conductivity λ_{bg} in the anomalous region and total conductivity value outside the extended critical region defined by [25]

$$|\Delta T^*| \leq 1/3 \quad \text{and} \quad |\Delta\rho^*| \leq 2/3 \quad (8)$$

6. CONCLUSION

The thermal conductivity of methane has been measured in the range 120–400 K at pressures to 700 bar and correlated to within $\pm 3\%$ in the experimental range except in the anomalous critical region. Accurate measurements are needed in this region in order to develop a model for reliably estimating the anomalous conductivity $\Delta\lambda_{cr}$.

A thermal conductivity table has been prepared in terms of temperature (K) and pressure (bar) and can be obtained from the authors. This table does not include the anomalous contribution, but the grid points falling within the anomalous region are identified.

APPENDIX

The experimental data on the thermal conductivity of methane are collected in Table IV.

ACKNOWLEDGMENTS

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Table IV. Thermal Conductivity of Methane. The Experimental Data

| Serial # | Test ID # | T (K) | P (bar) | ρ ($\text{g} \cdot \text{cm}^{-3}$) | λ ($\text{mW} \cdot \text{m}^{-1} \cdot \text{K}^{-1}$) |
|----------|-----------|---------|-----------|--|---|
| 1 | CH4-001 | 139.92 | 600.85 | 0.4357 | 204.88 |
| 2 | CH4-002 | 140.07 | 600.85 | 0.4356 | 204.70 |
| 3 | CH4-003 | 139.95 | 500.88 | 0.4289 | 196.45 |
| 4 | CH4-004 | 139.97 | 500.88 | 0.4289 | 195.83 |
| 5 | CH4-005 | 140.00 | 400.91 | 0.4214 | 187.30 |
| 6 | CH4-006 | 140.01 | 400.87 | 0.4214 | 187.37 |
| 7 | CH4-007 | 140.09 | 300.93 | 0.4129 | 176.87 |
| 8 | CH4-008 | 140.00 | 300.93 | 0.4130 | 177.60 |
| 9 | CH4-009 | 120.08 | 100.91 | 0.4199 | 179.56 |
| 10 | CH4-010 | 120.01 | 100.91 | 0.4200 | 179.65 |
| 11 | CH4-011 | 120.08 | 100.91 | 0.4199 | 179.74 |
| 12 | CH4-012 | 119.90 | 200.89 | 0.4287 | 190.16 |
| 13 | CH4-013 | 119.89 | 200.89 | 0.4287 | 190.80 |
| 14 | CH4-014 | 120.04 | 300.86 | 0.4360 | 199.96 |
| 15 | CH4-015 | 119.91 | 300.86 | 0.4361 | 200.32 |
| 16 | CH4-016 | 119.94 | 400.91 | 0.4428 | 208.37 |
| 17 | CH4-017 | 119.86 | 400.91 | 0.4429 | 209.33 |
| 18 | CH4-018 | 121.01 | 500.88 | 0.4480 | 212.99 |
| 19 | CH4-019 | 139.90 | 200.89 | 0.4034 | 166.96 |
| 20 | CH4-020 | 139.93 | 200.89 | 0.4034 | 166.32 |
| 21 | CH4-021 | 139.89 | 100.91 | 0.3917 | 154.05 |
| 22 | CH4-022 | 139.89 | 100.91 | 0.3917 | 154.20 |
| 23 | CH4-023 | 139.89 | 100.91 | 0.3917 | 153.85 |
| 24 | CH4-024 | 139.92 | 50.86 | 0.3846 | 147.09 |
| 25 | CH4-025 | 139.90 | 50.86 | 0.3846 | 147.19 |
| 26 | CH4-026 | 139.95 | 25.83 | 0.3806 | 143.24 |
| 27 | CH4-027 | 139.95 | 25.83 | 0.3806 | 143.39 |
| 28 | CH4-028 | 159.93 | 25.83 | 0.3402 | 115.33 |
| 29 | CH4-029 | 159.94 | 25.83 | 0.3401 | 115.08 |
| 30 | CH4-030 | 159.90 | 200.89 | 0.3763 | 143.77 |
| 31 | CH4-031 | 159.89 | 200.89 | 0.3763 | 143.74 |
| 32 | CH4-032 | 159.96 | 300.86 | 0.3890 | 156.17 |
| 33 | CH4-033 | 159.98 | 300.86 | 0.3890 | 155.82 |
| 34 | CH4-034 | 159.98 | 100.91 | 0.3591 | 129.31 |
| 35 | CH4-035 | 159.98 | 100.91 | 0.3591 | 129.16 |
| 36 | CH4-036 | 159.98 | 50.86 | 0.3475 | 120.29 |
| 37 | CH4-037 | 160.01 | 50.86 | 0.3474 | 119.94 |
| 38 | CH4-038 | 160.04 | 25.83 | 0.3399 | 115.18 |
| 39 | CH4-039 | 160.00 | 25.83 | 0.3400 | 114.93 |
| 40 | CH4-040 | 160.00 | 400.91 | 0.3995 | 166.74 |
| 41 | CH4-041 | 160.00 | 400.91 | 0.3995 | 166.64 |
| 42 | CH4-042 | 160.00 | 500.81 | 0.4086 | 176.81 |
| 43 | CH4-043 | 159.95 | 500.81 | 0.4087 | 176.98 |
| 44 | CH4-044 | 159.98 | 600.85 | 0.4167 | 185.53 |
| 45 | CH4-045 | 159.97 | 600.85 | 0.4167 | 185.80 |
| 46 | CH4-046 | 160.05 | 700.83 | 0.4238 | 193.60 |

Table IV. (Continued) Thermal Conductivity of Methane. The Experimental Data

| Serial # | Test ID# | T (K) | P (bar) | ρ ($\text{g} \cdot \text{cm}^{-3}$) | λ ($\text{mW} \cdot \text{m}^{-1} \cdot \text{K}^{-1}$) |
|----------|----------|---------|-----------|--|---|
| 47 | CH4-047 | 159.94 | 700.83 | 0.4239 | 194.17 |
| 48 | CH4-048 | 179.96 | 700.83 | 0.4060 | 176.98 |
| 49 | CH4-049 | 180.00 | 700.83 | 0.4060 | 177.06 |
| 50 | CH4-050 | 179.91 | 600.85 | 0.3977 | 168.28 |
| 51 | CH4-051 | 179.96 | 500.88 | 0.3882 | 158.37 |
| 52 | CH4-052 | 179.92 | 400.91 | 0.3773 | 148.17 |
| 53 | CH4-053 | 179.95 | 300.86 | 0.3640 | 136.53 |
| 54 | CH4-054 | 180.00 | 200.89 | 0.3467 | 122.91 |
| 55 | CH4-055 | 179.98 | 200.89 | 0.3467 | 122.79 |
| 56 | CH4-056 | 179.98 | 100.84 | 0.3201 | 106.00 |
| 57 | CH4-057 | 179.98 | 100.84 | 0.3201 | 105.83 |
| 58 | CH4-058 | 179.98 | 50.86 | 0.2948 | 93.92 |
| 59 | CH4-059 | 179.99 | 50.86 | 0.2948 | 94.16 |
| 60 | CH4-060 | 199.99 | 700.83 | 0.3882 | 161.18 |
| 61 | CH4-061 | 200.01 | 600.85 | 0.3787 | 152.39 |
| 62 | CH4-062 | 200.01 | 600.85 | 0.3787 | 152.44 |
| 63 | CH4-063 | 200.01 | 500.88 | 0.3677 | 142.54 |
| 64 | CH4-064 | 200.00 | 400.91 | 0.3545 | 131.59 |
| 65 | CH4-065 | 199.99 | 300.75 | 0.3380 | 119.76 |
| 66 | CH4-066 | 199.99 | 200.89 | 0.3145 | 104.91 |
| 67 | CH4-067 | 200.00 | 100.91 | 0.2674 | 84.95 |
| 68 | CH4-068 | 199.99 | 100.91 | 0.2674 | 84.65 |
| 69 | CH4-069 | 199.99 | 50.86 | 0.0925 | 40.15 |
| 70 | CH4-070 | 220.02 | 700.83 | 0.3708 | 147.79 |
| 71 | CH4-071 | 220.00 | 700.83 | 0.3709 | 147.89 |
| 72 | CH4-072 | 220.05 | 600.85 | 0.3600 | 139.11 |
| 73 | CH4-073 | 220.01 | 500.88 | 0.3474 | 128.97 |
| 74 | CH4-074 | 220.05 | 400.91 | 0.3318 | 118.07 |
| 75 | CH4-075 | 220.11 | 300.86 | 0.3111 | 105.42 |
| 76 | CH4-076 | 220.00 | 200.89 | 0.2793 | 89.67 |
| 77 | CH4-077 | 220.03 | 100.84 | 0.1890 | 66.15 |
| 78 | CH4-078 | 240.02 | 700.83 | 0.3539 | 137.42 |
| 79 | CH4-079 | 240.06 | 600.85 | 0.3418 | 128.56 |
| 80 | CH4-080 | 240.00 | 500.88 | 0.3274 | 118.30 |
| 81 | CH4-081 | 240.00 | 400.91 | 0.3093 | 106.96 |
| 82 | CH4-082 | 240.00 | 300.86 | 0.2843 | 94.38 |
| 83 | CH4-083 | 240.06 | 200.89 | 0.2423 | 78.35 |
| 84 | CH4-084 | 260.03 | 700.83 | 0.3375 | 128.14 |
| 85 | CH4-085 | 260.00 | 600.85 | 0.3242 | 119.20 |
| 86 | CH4-086 | 260.00 | 500.88 | 0.3081 | 109.25 |
| 87 | CH4-087 | 260.03 | 400.91 | 0.2873 | 98.59 |
| 88 | CH4-088 | 260.05 | 300.93 | 0.2579 | 86.20 |
| 89 | CH4-089 | 300.18 | 700.83 | 0.3068 | 114.95 |
| 90 | CH4-090 | 299.33 | 700.83 | 0.3075 | 115.72 |
| 91 | CH4-091 | 300.06 | 700.83 | 0.3069 | 114.75 |
| 92 | CH4-092 | 300.08 | 700.83 | 0.3069 | 114.55 |

Table IV. (Continued) Thermal Conductivity of Methane. The Experimental Data

| Serial # | Test ID# | T (K) | P (bar) | ρ ($\text{g} \cdot \text{cm}^{-3}$) | λ ($\text{mW} \cdot \text{m}^{-1} \cdot \text{K}^{-1}$) |
|----------|----------|---------|-----------|--|---|
| 93 | CH4-093 | 300.00 | 600.85 | 0.2913 | 106.00 |
| 94 | CH4-094 | 300.01 | 600.85 | 0.2913 | 106.39 |
| 95 | CH4-095 | 300.00 | 500.81 | 0.2720 | 97.09 |
| 96 | CH4-096 | 300.03 | 500.81 | 0.2720 | 97.22 |
| 97 | CH4-097 | 300.03 | 400.91 | 0.2468 | 86.59 |
| 98 | CH4-098 | 300.05 | 400.91 | 0.2468 | 86.64 |
| 99 | CH4-099 | 299.97 | 300.86 | 0.2112 | 74.99 |
| 100 | CH4-100 | 299.97 | 300.86 | 0.2112 | 75.09 |
| 101 | CH4-101 | 299.96 | 200.89 | 0.1560 | 60.81 |
| 102 | CH4-102 | 300.04 | 200.89 | 0.1559 | 61.01 |
| 103 | CH4-103 | 300.00 | 100.84 | 0.0759 | 43.04 |
| 104 | CH4-104 | 299.93 | 100.84 | 0.0759 | 43.14 |
| 105 | CH4-105 | 300.24 | 50.86 | 0.0356 | 35.13 |
| 106 | CH4-106 | 299.66 | 50.86 | 0.0357 | 35.33 |
| 107 | CH4-107 | 299.87 | 50.86 | 0.0357 | 35.73 |
| 108 | CH4-108 | 300.00 | 50.86 | 0.0356 | 35.81 |
| 109 | CH4-109 | 320.02 | 700.83 | 0.2929 | 110.32 |
| 110 | CH4-110 | 320.07 | 700.83 | 0.2928 | 110.47 |
| 111 | CH4-111 | 320.00 | 600.85 | 0.2762 | 101.51 |
| 112 | CH4-112 | 319.95 | 600.85 | 0.2763 | 101.96 |
| 113 | CH4-113 | 319.95 | 500.88 | 0.2558 | 92.80 |
| 114 | CH4-114 | 319.94 | 500.88 | 0.2558 | 92.60 |
| 115 | CH4-115 | 319.98 | 400.91 | 0.2291 | 83.05 |
| 116 | CH4-116 | 319.98 | 400.91 | 0.2291 | 82.90 |
| 117 | CH4-117 | 319.96 | 300.86 | 0.1922 | 72.75 |
| 118 | CH4-118 | 319.98 | 300.86 | 0.1921 | 71.86 |
| 119 | CH4-119 | 320.06 | 200.89 | 0.1389 | 59.19 |
| 120 | CH4-120 | 320.04 | 200.89 | 0.1389 | 59.19 |
| 121 | CH4-121 | 319.98 | 100.91 | 0.0683 | 44.92 |
| 122 | CH4-122 | 320.00 | 100.91 | 0.0683 | 44.79 |
| 123 | CH4-123 | 339.80 | 700.83 | 0.2798 | 106.60 |
| 124 | CH4-124 | 339.96 | 100.91 | 0.0623 | 47.18 |
| 125 | CH4-125 | 339.98 | 100.91 | 0.0623 | 47.67 |
| 126 | CH4-126 | 340.00 | 100.91 | 0.0623 | 47.67 |
| 127 | CH4-127 | 340.05 | 700.83 | 0.2796 | 106.05 |
| 128 | CH4-128 | 340.02 | 700.83 | 0.2796 | 105.66 |
| 129 | CH4-129 | 340.00 | 600.85 | 0.2622 | 98.53 |
| 130 | CH4-130 | 340.02 | 600.85 | 0.2622 | 98.39 |
| 131 | CH4-131 | 339.98 | 500.88 | 0.2407 | 90.13 |
| 132 | CH4-132 | 339.96 | 400.91 | 0.2132 | 81.33 |
| 133 | CH4-133 | 339.95 | 300.86 | 0.1762 | 71.26 |
| 134 | CH4-134 | 340.23 | 200.89 | 0.1255 | 58.67 |
| 135 | CH4-135 | 400.15 | 700.83 | 0.2449 | 102.24 |
| 136 | CH4-136 | 400.07 | 600.85 | 0.2261 | 95.35 |

Table IV. (Continued) Thermal Conductivity of Methane. The Experimental Data

| Serial # | Test ID# | T (K) | P (bar) | ρ ($\text{g} \cdot \text{cm}^{-3}$) | λ ($\text{mW} \cdot \text{m}^{-1} \cdot \text{K}^{-1}$) |
|----------|----------|---------|-----------|--|---|
| 137 | CH4-137 | 399.99 | 500.88 | 0.2036 | 87.89 |
| 138 | CH4-138 | 399.95 | 400.91 | 0.1759 | 79.47 |
| 139 | CH4-139 | 399.92 | 300.86 | 0.1416 | 71.29 |
| 140 | CH4-140 | 399.88 | 200.89 | 0.0991 | 63.87 |
| 141 | CH4-141 | 399.89 | 100.91 | 0.0502 | 54.03 |
| 142 | CH4-142 | 379.92 | 700.83 | 0.2557 | 102.25 |
| 143 | CH4-143 | 379.97 | 600.85 | 0.2372 | 95.98 |
| 144 | CH4-144 | 379.98 | 500.88 | 0.2147 | 88.08 |
| 145 | CH4-145 | 380.03 | 400.91 | 0.1867 | 79.98 |
| 146 | CH4-146 | 379.97 | 400.91 | 0.1868 | 79.93 |
| 147 | CH4-147 | 379.99 | 300.93 | 0.1514 | 71.16 |
| 148 | CH4-148 | 380.09 | 200.89 | 0.1063 | 61.76 |
| 149 | CH4-149 | 379.91 | 100.91 | 0.0536 | 52.97 |
| 150 | CH4-150 | 359.90 | 700.83 | 0.2673 | 104.39 |
| 151 | CH4-151 | 357.90 | 700.83 | 0.2685 | 104.54 |
| 152 | CH4-152 | 359.89 | 600.85 | 0.2492 | 96.62 |
| 153 | CH4-153 | 359.89 | 500.88 | 0.2272 | 89.34 |
| 154 | CH4-154 | 359.90 | 400.91 | 0.1992 | 80.52 |
| 155 | CH4-155 | 359.89 | 300.93 | 0.1628 | 70.68 |
| 156 | CH4-156 | 359.91 | 200.89 | 0.1150 | 60.69 |
| 157 | CH4-157 | 359.94 | 200.89 | 0.1150 | 60.69 |
| 158 | CH4-158 | 359.94 | 100.98 | 0.0576 | 50.07 |
| 159 | CH4-159 | 260.58 | 700.83 | 0.3371 | 129.47 |
| 160 | CH4-160 | 260.51 | 600.85 | 0.3238 | 119.32 |
| 161 | CH4-161 | 260.48 | 500.88 | 0.3076 | 109.35 |
| 162 | CH4-162 | 260.53 | 400.91 | 0.2868 | 98.79 |
| 163 | CH4-163 | 260.57 | 300.86 | 0.2572 | 86.61 |
| 164 | CH4-164 | 260.71 | 200.96 | 0.2062 | 71.73 |
| 165 | CH4-165 | 260.90 | 150.90 | 0.1618 | 60.45 |
| 166 | CH4-166 | 261.15 | 200.96 | 0.2055 | 70.62 |
| 167 | CH4-167 | 261.17 | 100.84 | 0.1011 | 46.18 |
| 168 | CH4-168 | 261.69 | 50.86 | 0.0437 | 32.65 |
| 169 | CH4-169 | 261.93 | 50.86 | 0.0436 | 32.45 |
| 170 | CH4-170 | 277.15 | 700.83 | 0.3241 | 122.16 |
| 171 | CH4-171 | 277.31 | 600.85 | 0.3096 | 113.22 |
| 172 | CH4-172 | 277.43 | 500.81 | 0.2919 | 103.41 |
| 173 | CH4-173 | 277.72 | 400.91 | 0.2687 | 93.36 |
| 174 | CH4-174 | 277.98 | 300.86 | 0.2356 | 81.06 |
| 175 | CH4-175 | 278.28 | 200.89 | 0.1804 | 65.16 |
| 176 | CH4-176 | 278.52 | 150.90 | 0.1382 | 55.87 |
| 177 | CH4-177 | 279.19 | 100.84 | 0.0869 | 44.47 |
| 178 | CH4-178 | 279.51 | 50.93 | 0.0395 | 35.72 |
| 179 | CH4-179 | 279.63 | 51.00 | 0.0395 | 35.72 |
| 180 | CH4-180 | 279.99 | 100.84 | 0.0864 | 44.61 |

NOMENCLATURE

| | |
|-----------------------------|---|
| a_k, b_{ij}, b_k | Parameters of the regression model, $k = 0$ to n ; $i = 0$ to m ; $j = 0$ to n |
| P | Pressure (MPa or bar) |
| Q_l | Heat flux per unit length ($\text{mW} \cdot \text{m}^{-1}$) |
| t | time (s) |
| T | Temperature (K) |
| T_{cr} | Critical temperature (K) |
| T_r | reduced temperature ($= T/T_{\text{cr}}$) |
| ΔT_w | Temperature rise of wire between times t_1 and t_2 (deg K) |
| ΔT^* | Reduced temperature difference $(T - T_{\text{cr}})/T_{\text{cr}}$ |
| λ | Thermal conductivity ($\text{mW} \cdot \text{m}^{-1} \cdot \text{K}^{-1}$) |
| λ_1 | Thermal conductivity at 1 bar ($\text{mW} \cdot \text{m}^{-1} \cdot \text{K}^{-1}$) |
| λ_{bg} | Background thermal conductivity ($\text{mW} \cdot \text{m}^{-1} \cdot \text{K}^{-1}$) |
| $\Delta\lambda_{\text{cr}}$ | Anomalous thermal conductivity ($\text{mW} \cdot \text{m}^{-1} \cdot \text{K}^{-1}$) |
| $\Delta\lambda_e$ | Excess thermal conductivity ($\text{mW} \cdot \text{m}^{-1} \cdot \text{K}^{-1}$) |
| ρ | Density ($\text{g} \cdot \text{cm}^{-3}$) |
| ρ_{cr} | Critical density ($\text{g} \cdot \text{cm}^{-3}$) |
| ρ_r | Reduced density ($= \rho/\rho_{\text{cr}}$) |
| $\Delta\rho^*$ | Reduced density difference $(\rho - \rho_{\text{cr}})/\rho_{\text{cr}}$ |

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